



PATENT

Attorney's Docket No.: U 012932-5

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Box Patent Application
 Assistant Commissioner for Patents
 Washington, D.C. 20231



NEW APPLICATION TRANSMITTAL

Transmitted herewith for filing is the patent application of Inventors:

1. SONTI VENKATA RAMAKRISHNA
2. SRENIVASULUREDDY VENKATA MOHAN
3. REDDY SHETTY PRAKASHAM
4. PALLE KOMARAIHAH
5. KONDAPURAM VIJAYA RAGHAVAN

WARNING: *The Declaration must name all of the actual inventor(s).*

For (title):

METHOD FOR THE PREPARATION OF STABLE AND REUSABLE BIOSENSING GRANULES

1. Type of Application

This new application is for a(n) (check one applicable item below):

- ☒ Original (nonprovisional)
- ☐ Design
- ☐ Plant

WARNING: *Do not use this transmittal for a completion in the U.S. of an International Application under 35 U.S.C. 371(c)(4) unless the International Application is being filed as a divisional, continuation or continuation-in-part application.*

CERTIFICATION UNDER 37 CFR 1.10

I hereby certify that this New Application Transmittal and the documents referred to as enclosed therein are being deposited with the United States Postal Service on this date **AUGUST 31, 2000** in an envelope as "Express Mail Post Office to Addressee" Mailing Label Number EL699731305US addressed to the: Assistant Commissioner of Patents, Washington, D.C. 20231

GERALDINE MARTI

(type or print name of person mailing paper)

(Signature of person mailing paper)

NOTE: *Each paper or fee referred to as enclosed herein has the number of the "Express Mail" mailing label placed thereon prior to mailing. 37 CFR 1.10(b).*

WARNING: *Certificate of mailing (first class) or facsimile transmission procedures of 37 CFR 1.8 cannot be used to obtain a date of mailing or transmission for this correspondence.*

(Application Transmittal [4-1]—page 1 of 7)

EXPRESS MAIL LABEL
 NO.: EL699731163US

WARNING: Do not use this transmittal for the filing of a provisional application.

2. Benefit of Prior U.S. Application(s) (35 U.S.C. 119(e), 120, or 121)

NOTE: If the new application being transmitted is a divisional, continuation or a continuation-in-part of a parent case, or where the parent case is an International Application which designated the U.S., or benefit of a prior provisional application is claimed, then check the following item and complete and attach **ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION(S) CLAIMED**.

WARNING: If an application claims the benefit of the filing date of an earlier filed application under 35 U.S.C. 120, 121 or 365(c), the 20-year term of that application will be based upon the filing date of the earliest U.S. application that the application makes reference to under 35 U.S.C. 120, 121 or 365(c). (35 U.S.C. 154(a)(2) does not take into account, for the determination of the patent term, any application on which priority is claimed under 35 U.S.C. 119, 365(a) or 365(b).) For a c-i-p application, applicant should review whether any claim in the patent that will issue is supported by an earlier application and, if not, the applicant should consider canceling the reference to the earlier filed application. The term of a patent is not based on a claim-by-claim approach. See Notice of April 14, 1995, 60 Fed. Reg. 20,195, at 20,205.

WARNING: When the last day of pendency of a provisional application falls on a Saturday, Sunday, or Federal holiday within the District of Columbia, any nonprovisional application claiming benefit of the provisional **must** be filed prior to the Saturday, Sunday or Federal holiday within the District of Columbia. See 37 C.F.R. § 1.78(a)(3).

- ☐ The new application being transmitted claims the benefit of prior U.S. application(s) and enclosed are **ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION(S) CLAIMED**.

NOTE: If one of the following 3 items apply, then complete and attach **ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF A PRIOR U.S. APPLICATION CLAIMED** and a **NOTIFICATION IN PARENT APPLICATION OF THE FILING OF THIS CONTINUATION APPLICATION**.

- ☐ Divisional.
☐ Continuation.
☐ Continuation-in-Part (C-I-P).

3. Papers Enclosed That Are Required For Filing Date Under 37 CFR 1.53 (Regular) or 37 CFR 1.153 (Design) Application

11 Pages of specification

3 Pages of claims

1 Pages of Abstract

 Sheets of drawing

- ☐ formal
☐ informal

WARNING: **DO NOT** submit original drawings. A high quality copy of the drawings should be supplied when filing a patent application. The drawings that are submitted to the Office must be on strong, white, smooth, and non-shiny paper and meet the standards according to § 1.84. If corrections to the drawings are necessary, they should be made to the original drawing and a high-quality copy of the corrected original drawing then submitted to the Office. Only one copy is required or desired. Comments on proposed new 37 CFR 1.84. Notice of March 9, 1988 (1990 O.G. 57-62).

NOTE: "Identifying indicia, if provided, should include the application number or the title of the invention, inventor's name, docket number (if any), and the name and telephone number of a person to call if the Office is unable to match the drawings to the proper application. This information should be placed on the back of each sheet of drawing a minimum distance of 1.5 cm. (5/8 inch) down from the top of the page." 37 C.F.R. 1.84(c).

(complete the following, if applicable)

- ☐ The enclosed drawing(s) are photograph(s), and there is also attached a "PETITION TO ACCEPT PHOTOGRAPH(S) AS DRAWING(S)". 37 C.F.R. 1.84(b).

4. Additional papers enclosed

- ☐ Preliminary Amendment
- ☐ Information Disclosure Statement (37 CFR 1.98)
- ☐ Form PTO-1449
- ☐ Citations
- ☐ Declaration of Biological Deposit
- ☐ Submission of "Sequence Listing," computer readable copy and/or amendment pertaining thereto for biotechnology invention containing nucleotide and/or amino acid sequence.
- ☐ Authorization of Attorney(s) to Accept and Follow Instructions from Representative
- ☐ Special Comments
- ☐ Other

5. Declaration or oath

- ☐ Enclosed
- executed by (*check all applicable boxes*)
- ☐ inventors.
- ☐ legal representative of inventors. 37 CFR 1.42 or 1.43
- ☐ joint inventor or person showing a proprietary interest on behalf of inventor who refused to sign or cannot be reached.
- ☐ This is the petition required by 37 CFR 1.47 and the statement required by 37 CFR 1.47 is also attached. *See item 13 below for fee.*
- ☒ Not Enclosed.

WARNING: *Where the filing is a completion in the U.S. of an International Application but where a declaration is not available or where the completion of the U.S. application contains subject matter in addition to the International Application the application may be treated as a continuation or continuation-in-part, as the case may be, utilizing ADDED PAGE FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION CLAIMED.*

- ☒ Application is made by a person authorized under 37 CFR 1.41(c) on behalf of *all the above named inventors*. (The declaration or oath, along with the surcharge required by 37 CFR 1.16(e) can be filed subsequently).

NOTE: *It is important that all the correct inventor(s) are named for filing under 37 CFR 1.41(c) and 1.53(b).*

- ☐ Showing that the filing is authorized. (*Not required unless called into question. 37 CFR 1.41(d).*)

6. Inventorship Statement

WARNING: *If the named inventors are each not the inventors of all the claims an explanation, including the ownership of the various claims at the time the last claimed invention was made, should be submitted.*

The inventorship for all the claims in this application are:

- ☐ The same
- ☐ Not the same. An explanation, including the ownership of the various claims at the time the last claimed invention was made,

7. Language

NOTE: An application including a signed oath or declaration may be filed in a language other than English. A verified English translation of the non-English language application and the processing fee of \$130.00 required by 37 CFR 1.17(k) is required to be filed with the application or within such time as may be set by the Office. 37 CFR 1.52(d).

NOTE: A non-English oath or declaration in the form provided or approved by the PTO need not be translated. 37 CFR 1.69(b).

- ☒ English
- ☐ non-English
- ☐ the attached translation is a verified translation. 37 CFR 1.52(d).

8. Assignment

- ☒ An assignment of the invention to COUNCIL OF SCIENTIFIC & INDUSTRIAL RESEARCH
- ☐ is attached. A separate ☐ "COVER SHEET FOR ASSIGNMENT (DOCUMENT) ACCOMPANYING NEW PATENT APPLICATION" or ☐ FORM PTO 1595 is also attached.
- ☒ will follow.

NOTE: "If an assignment is submitted with a new application, send two separate letters—one for the application and one for the assignment." Notice of May 4, 1990 (1114 O.G. 77-78).

WARNING: A newly executed "CERTIFICATE UNDER 37 CFR 3.73(b)" must be filed when a continuation-in-part application is filed by an assignee. Notice of April 30, 1993. 1150 O.G. 62-64.

9. Certified Copy

Certified copy of application

Country

Appln. No.

Filed

from which priority is claimed

- ☐ is attached.
- ☐ will follow.

NOTE: The foreign application forming the basis for the claim for priority must be referred to in the oath or declaration. 37 CFR 1.55(a) and 1.63.

NOTE: This item is for any foreign priority for which the application being filed directly relates. If any parent U.S. application or International Application from which this application claims benefit under 35 U.S.C. 120 is itself entitled to priority from a prior foreign application then complete item 18 on the ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION(S) CLAIMED.

10. Fee Calculation (37 CFR 1.16)

- A. ☒ Regular Application

Claims as Filed

Number Filed	Number Extra	Rate	Basic Fee 37 CFR 1.16(a) \$690.00
Total Claims (37 CFR 1.16(c))	19 - 20 = 0 x \$	18.00	
Independent Claims (37 CFR 1.16(b))	1 - 3 = 0 x \$	78.00	
Multiple dependent claim(s), if any (37 CFR 1.16(d))	+ \$	260.00	

- ☐ Amendment cancelling extra claims enclosed.
- ☐ Amendment deleting multiple-dependencies enclosed.
- ☐ Fee for extra claims is not being paid at this time.

NOTE: *If the fees for extra claims are not paid on filing they must be paid or the claims cancelled by amendment, prior to the expiration of the time period set for response by the Patent and Trademark Office in any notice of fee deficiency. 37 CFR 1.16(d).*

Filing Fee Calculation \$

- B. ☐ Design application
(\$310.00 — 37 CFR 1.16(f))

Filing Fee Calculation \$

- C. ☐ Plant application
(\$480.00 — 37 CFR 1.16(g))

Filing Fee Calculation \$

11. Small Entity Statement(s)

- ☐ Verified Statement(s) that this is a filing by a small entity under 37 CFR 1.9 and 1.27 is(are) attached or has been filed.

Filing Fee Calculation (50% of **A**, **B** or **C** above) \$

NOTE: *Any excess of the full fee paid will be refunded if a verified statement and a refund request are filed within 2 months of the date of timely payment of a full fee. 37 CFR 1.28(a).*

12. Request for International-Type Search (37 CFR 1.104(d)) (Complete, if applicable)

- ☐ Please prepare an international-type search report for this application at the time when national examination on the merits takes place.

13. Fee Payment Being Made At This Time

- ☒ Not Enclosed
- ☒ No filing fee is to be paid at this time. *(This and the surcharge required by 37 CFR 1.16(e) can be paid subsequently.)*

- ☐ Enclosed

☐ basic filing fee \$

- ☐ Recording assignment
(\$40.00; 37 CFR 1.21(h)) (See attached "COVER SHEET FOR ASSIGNMENT ACCOMPANYING NEW APPLICATION.")
- ☐ Petition fee for filing by other than all the inventors or person on behalf of the inventor where inventor refused to sign or cannot be reached.
(\$130.00; 37 CFR 1.47 and 1.17(h)) \$
- ☐ For processing an application with a specification in a non-English language.
(\$130.00; 37 CFR 1.52(d) and 1.17(k)) \$
- ☐ Processing and retention fee
(\$130.00; 37 CFR 1.53(d) and 1.21(l))
- ☐ Fee for international-type search report
(\$40.00; 37 CFR 1.21(e)). \$

NOTE: 37 CFR 1.21(l) establishes a fee for processing and retaining any application which is abandoned for failing to complete the application pursuant to 37 CFR 1.53(d) and this, as well as the changes to 37 CFR 1.53 and 1.78, indicate that in order to obtain the benefit of a prior U.S. application, either the basic filing fee must be paid or the processing and retention fee of §1.21(l) must be paid within 1 year from notification under §53(d).

Total fees enclosed \$

14. Method of Payment of Fees

- ☐ Check in the amount of \$
- ☐ Charge Account No. 12-0425 in the amount of \$

A duplicate of this transmittal is attached.

NOTE: Fees should be itemized in such a manner that it is clear for which purpose the fees are paid. 37 CFR 1.22(b).

15. Authorization to Charge Additional Fees

WARNING: If no fees are to be paid on filing, the following items should not be completed.

WARNING: Accurately count claims, especially multiple dependent claims, to avoid unexpected high charges, if extra claim charges are authorized.

- ☐ The Commissioner is hereby authorized to charge the following additional fees by this paper and during the entire pendency of this application to Account No. 12-0425.
 - ☐ 37 CFR 1.16(a), (f) or (g) (filing fees)
 - ☐ 37 CFR 1.16(b), (c) and (d) (presentation of extra claims)

NOTE: Because additional fees for excess or multiple dependent claims not paid on filing or on later presentation must only be paid or these claims cancelled by amendment prior to the expiration of the time period set for response by the PTO in any notice of fee deficiency (37 CFR 1.16(d)), it might be best not to authorize the PTO to charge additional claim fees, except possibly when dealing with amendments after final action.

- ☐ 37 CFR 1.16(e) (surcharge for filing the basic filing fee and/or declaration on a date later than the filing date of the application)
- ☐ 37 CFR 1.17 (application processing fees)

WARNING: While 37 CFR 1.17(a), (b), (c) and (d) deal with extensions of time under §1.136(a), this authorization should be made only with the knowledge that: "Submission of the appropriate extension fee under 37 C.F.R. 1.136(a) is to no avail unless a request or petition for extension is filed." (Emphasis added). Notice of November 5, 1985 (1060 O.G. 27)

- ☐ 37 CFR 1.18 (issue fee at or before mailing of Notice of Allowance, pursuant to 37 CFR 1.311(b))

NOTE: Where an authorization to charge the issue fee to a deposit account has been filed before the mailing of a Notice of Allowance, the issue fee will be automatically charged to the deposit account at the time of mailing the notice of allowance. 37 CFR 1.311(b).

NOTE: 37 CFR 1.28(b) requires "Notification of any change in loss of entitlement to small entity status must be filed in the application ... prior to paying, or at the time of paying, ... issue fee". From the wording of 37 CFR 1.28(b): (a) notification of change of status must be made even if the fee is paid as "other than a small entity" and (b) no notification is required if the change is to another small entity.

16. Instructions As To Overpayment

- ☐ credit Account No. 12-0425
☐ refund



Signature of Attorney

Reg. No.25,858

Tel. No. (212) 708-1930

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NEW YORK, NEW YORK 10023

☐ **Incorporation by reference of added pages**

(Check the following item if the application in this transmittal claims the benefit of prior U.S. application(s) (including an international application entering the U.S. stage as a continuation, divisional or C-I-P application) and complete and attach the ADDED PAGES FOR NEW APPLICATION TRANSMITTAL WHERE BENEFIT OF PRIOR U.S. APPLICATION(S) CLAIMED)

- ☐ Plus Added Pages for New Application Transmittal Where Benefit of Prior U.S. Application(s) Claimed

Number of pages added ____

- ☐ Plus Added Pages for Papers Referred to in Item 4 Above

Number of pages added ____

- ☐ Plus "Assignment Cover Letter Accompanying New Application"

Number of pages added ____

☒ **Statement Where No Further Pages Added**

(If no further pages form a part of this Transmittal, then end this Transmittal with this page and check the following item:)

- ☒ This transmittal ends with this page.

U 012932-5

METHOD FOR THE PREPARATION OF STABLE AND REUSABLE BIOSENSING GRANULES**Field of the invention**

The present invention relates to a method for the preparation of stable and reusable biosensing granules useful for assessing the biotreatability of effluents.

Background of the invention

The present invention of development of biosensing granules will help in rapid characterisation of any effluent at on-site. Moreover, the invented biosensing granules are reusable for several times and involve less manpower. In addition, these biosensing granules are ecofriendly in nature, cost-effective and do not require any chemical or energy input and are hence easy to operate at field conditions.

The byproduct liquid streams from various industries contain different environmentally undesirable chemical compounds that adversely affect water bodies and groundwater reservoirs. The reduction of organic pollutants to environmentally acceptable limits is essential before discharging these effluents into the environment. This requires a prerequisite of measurement of organic content in these discharges, which help in estimation of pollutant strength, design of treatment methodology and disposable alternative, etc. The biodegradable organic strength in an effluent can be determined by calculating the ratio of biological oxygen demand (BOD) to chemical oxygen demand (COD). The prolonged time of analysis, undependable simulated experimental conditions and toxic nature of effluents limits its utilisation and subsequent decision making for selection of appropriate treatment methodology at on-site.

Effluent treatment options can be generally divided into the following categories – physical, chemical, biological and thermal. Among the above categories, biological treatment processes possess an edge over the others due to its potential to degrade the organic pollutants into simple and environmentally safe compounds such as methane, carbon dioxide and water that are eco-friendly in nature. Biotreatment of an effluent can be done by inoculation of appropriate microbial consortia and incubating either in anaerobic or aerobic conditions. Under aerobic conditions, microbial consorts present in the system utilise the oxygen and organic compounds of effluent for energy generation. The pollution concentration can be assessed by calculating the microbial activity in waste water. Thus, microbial activity in terms of respiration is an important indication to characterise the effluents under different biotreatability classes.

Several attempts have been made in part to determine the organic content of industrial effluents by chemical as well as by biological means so as to characterise the effluent, evaluate its biodegradability, and for choosing the appropriate treatment process option [Rogers, K. R. and Williams, L. R. (1995) Trends Anal. Chem. 14; 289 – 294]. The organic content of an effluent is generally expressed in terms of the amount of oxygen required to degrade the organic pollutants and is measured either by chemical or biological means. One of the thumb rules used in assessing the effluent's biotreatability criteria is the ratio of the biological oxygen demand (BOD) to that of the chemical oxygen demand (COD), which is normally a fraction. A low value of the BOD/COD ratio indicates the difficulty in biodegradation, while a high value represents the amicability of the wastes for biological degradation.

Biochemical oxygen demand is basically a bioassay procedure involving the estimation of oxygen consumed in a simulated system under standard prescribed conditions. BOD is performed in a BOD bottle of 300 ml capacity at 20°C for 5 days by taking suitable aliquots of effluents in the presence of seed, either from raw sewage or treated effluent from waste water treatment plant and nutrients. The long time taken for analysis, undependable simulated experimental conditions, and the toxic nature of effluents offsets its application. In this context, COD comes into existence where organic matter in the effluent was oxidised by a strong oxidising agent at elevated temperature under acidic environment. This test requires approximately 3 hours for analysis and is not dependant on biological environment. However, this method has its own limitations, such as undependable accuracy, input of chemicals and energy and production of secondary effluent disposing problems, etc. This process of BOD/COD characterisation of an effluent is time consuming, a laboratory installation with special instrumentation to maintain the required temperature constantly, input of chemicals and energy and can not be generally utilised in the field conditions.

The other wastewater characterisation techniques for biodegradability are measurement of its inorganic nitrogen compound uptake rates. However, these methods will be applicable only for certain types of wastes. Moreover, they require special instrumentation to measure the respective inorganic compounds in the effluents. Recently, efforts are being made to combine an already advanced respirometric technique, the hybrid respirometer with titrimetric technique with limited success [Vanrolleghem, P. A. and Spanjers, H. (1998) Wat. Sci. Technol., 37; 237 – 246]. Several other researchers have also attempted to develop micro-organism based biosensors, which involve determination of microbial activity either by spectrophotometrically or electrochemically [Bains, W. (1994) Biosensors Bioelectronics., 9;

111 – 117; Corbisier, P., Thiry, E., and Diels, L. (1996) *Environ. Toxicol. Water Qual.*, 11; 171 – 177; Silva, M. J., and Wong, J. L. (1995) *Bioelectrochem. Bioener.*, 37; 141 – 148]. The drawbacks with all these techniques are long incubation periods and low initial response, etc. [Rogers, K. R. and Koglin, E. N. (1997) in *Biosensors for Direct Monitoring of Environmental Pollution in Field*, (ed. D. P. Nikolelis, U. J. Krull, J. Wang, and M. Mascini) Kluwer Publishers, Boston, 335 – 349]. Moreover, implementation of these technologies for on-site effluent characterisation is not possible [Koglin, E. N. and Williams, L. R. (1994) *Trends. Anal. Chem.* 13; 294 – 299]. Hence the development of a reliable methodology to rapidly estimate the oxygen required for biodegradation considerably promises advancement in environmental monitoring.

Objects of the invention

The main object of the invention is to provide a process for the preparation of stable and reusable biosensing granules useful in measuring the biotreatability of effluents.

Another object of the invention is to provide a cost-effective process for the evaluation of the biotreatability of effluents.

It is a further object of the invention to provide a tool kit for the effective characterisation of the biotreatability of effluent under field conditions.

It is another object of the invention to provide a stable and reusable biosensing granules for determination of the biodegradable nature of an effluent.

It is a further object of the invention to provide information regarding discharge characters on site.

Yet another object of the invention is to provide a eco-friendly technique that does not require chemicals for waste characterization for biological treatment.

Another object of the invention is to provide a fast method to determine the biotreatability of an effluent.

Summary of the invention

Accordingly, the present invention provides a process for the preparation of stable and reusable biosensing granules useful in the assessment of biodegradability of effluents, said process comprising developing active aerobic microbial consortia in synthetic medium, separating the active aerobic microbial consortia, immobilising the said microbial consortia using natural polymer to form biosensing granules, dehydrating the immobilised biosensing granules at 24 - 32°C for a period of 4 – 12 hours, to obtain stable biosensing granules having a moisture content of 5 – 30 %.

The present invention also relates to a method for the preparation of stable and reusable biosensing granules useful for assessing the biotreatability of effluent which comprises.

- i. selecting a seed culture from raw sewage, wastewater treatment plants or activated sludge units;
- ii. preparing a synthetic growth media;
- iii. inoculating a microbial consortia in the said media;
- iv. incubating the microbial consortia under aerobic condition having an air flow of about 5 ml/minute, at about 28°C for a period of 12 – 24 hours or till the level of mixed liquor suspended solids (MLSS) reaches 14500 – 15500 mg/liter on a dry weight basis;
- v. separating the active aerobic microbial consortia by centrifugation at the appropriate rpm for 10 – 15 minutes and at a temperature of about 28°C;
- vi. immobilizing the said microbial consortia using aqueous natural polymer solution by any known methods to obtain immobilized biosensing beads;
- vii. separating the said biosensing beads by decanting the said solution;
- viii. washing the beads with water thoroughly several times;
- ix. dehydrating the beads at a temperature in the range of 24 - 36°C for a period of 2 – 20 hours to obtain stable biosensing granules having a moisture content of 5 – 30 %;
- x. activating the stable biosensing granules by incubation in 2 – 5 % (w/v) aqueous solution at 28°C for 2 – 10 hours to get active stable biosensing granules;
- xi. separating the active granules from the activation solution by conventional methods.

In one embodiment of the invention, the aerobic microbial consortia is collected from raw sewage, wastewater treatment plants or from activated aerated sludge units.

In another embodiment of the invention, the synthetic growth media used consists of (in grams/liter): glucose – 29 - 31; ammonium chloride – 5.5 – 7.5; potassium dihydrogen orthophosphate – 1.5 – 3.5; dipotassium hydrogen orthophosphate – 0.5 - 1.5; sodium bicarbonate – 4.5 – 5.5; yeast extract – 0.5 – 1.5; urea – 0.3 – 0.7; and tryptone – 0.5 – 1.5.

In another embodiment of the invention, the pH of the prepared synthetic growth media is adjusted to about 7.0 using 0.1 N hydrochloric acid or 0.1 N sodium hydroxide.

In another embodiment of the invention, about 10 % (w/v) of the collected microbial consortia is inoculated in the synthetic growth medium.

In a further embodiment of the invention, the inoculated synthetic growth medium is aerated by passing air at the rate of about 5 ml/minute.

In yet another embodiment of the invention, the growth media is incubated at a temperature of 24 - 32°C.

In another embodiment of the invention, the growth of the active aerobic microbial consortia is terminated after the mixed liquor suspended solids (MLSS) reaches 14500 - 15500 mg/liter.

In another embodiment of the invention, the active aerobic microbial consortia is separated from the broth using conventional methods selected from centrifugation, settling, decanting the supernatant.

In a further embodiment of the invention, the separated active aerobic microbial consortia is immobilized using 1 - 3 % (w/v) sodium alginate and 0.2M calcium chloride solution.

In yet another embodiment of the invention, the active aerobic microbial consortia is used for immobilisation in the range of 3 - 5 % (w/v) to obtain immobilized biosensing granules.

In another embodiment of the invention, the prepared immobilised biosensing granules are incubated for 12 - 24 hours at 4°C in 0.2 M calcium chloride solution.

In another embodiment of the invention, the prepared immobilised biosensing granules are separated from the calcium chloride solution by decanting the aqueous liquid.

In another embodiment of the invention, the immobilised biosensing granules are dehydrated at 24 - 32°C for a period of 2 - 20 hours to obtain stable biosensing granules with 5 - 30% moisture content.

In a further embodiment of the invention, the stable biosensing granules are incubated for 2 - 10 hours in 2 - 5 % (w/v) glucose solution, at 24 - 32°C to obtain active stable biosensing granules.

In yet another embodiment of the invention, the stable biosensing granules are separated from the activation media by draining out the solution.

In a further embodiment of the invention, the residual dissolved oxygen content of the effluent is measured using oxygen probe before and 2 - 6 hours of addition of activation stable biosensing granules in the range of from 2 - 5% (w/v).

The present invention also relates to a method for the estimation of the biotreatability of an effluent using the biosensing granules of claim 1 wherein the effluent is characterized as highly biotreatable if the dissolved oxygen consumption rate by the activated biosensing granules is more than 2 mg/l, medium when the said oxygen consumption rate is between 1.0 to 2.0 mg/l, and low when the oxygen consumption rate is less than 1.0 mg/l.

Detailed description of the invention

The biosensing granules of the invention are mechanically strong and biologically active and can be employed in assessing the biodegradability of the effluent within 2 – 4 hours at a temperature in the range of from 24 – 32°C without involving BOD instrumentation or COD analysis.

The process of the present invention involves the preparation of a stable and reusable biosensing granule and its use for assessing the biotreatability of effluents. The seed culture is selected from raw sewage, wastewater treatment plant or from activated sludge unit. A synthetic growth media consisting of (in grams/liter): glucose – 30.0; ammonium chloride – 6.5; potassium dihydrogen orthophosphate – 2.5; dipotassium hydrogen orthophosphate – 1.0; sodium bicarbonate – 5.5; yeast extract – 1.0; urea – 0.5; and tryptone – 1.0 at pH 7.0 is prepared, under aerated condition having air flow of 5 ml/minute, at 28°C for a period of 12 – 24 hours or till the mixed liquor suspended solids (MLSS) reaches 14500 – 15500 mg/liter on a dry weight basis. The resultant active aerobic microbial consortia was separated by centrifugation at an appropriate rpm, preferably 10000 rpm for 10 – 15 minutes at 28°C. The said microbial consortia is immobilised using aqueous natural polymer solution by known methods to obtain immobilised microbial biosensing beads. These beads are separated by decanting the solution and washed thoroughly with water several times and dehydrated at a temperature in the range of from 24 – 36°C for a period of 2 – 20 hours to obtain stable biosensing granules having moisture in the range of from 5 – 30 %.

The stable and reusable biosensing granules of the invention are granular spherical particles having a diameter of 0.3 – 1.0 mm, blackish in colour, hard, robust particles which are insoluble in aqueous or organic medium. These granules have intrinsic capacity to absorb or desorb water molecules. These stable granules are activated by incubating them in 2 – 5 % (w/v) aqueous solution at 28°C for 2 – 10 hours to get active stable biosensing granules. These active granules are separated from the activation solution by conventional methods. Various types of industrial effluents are collected from industrial sites and incubated at about 1 – 5 % (w/v) to obtain active stable biosensing granules. The dissolved oxygen in the effluent is measured before the addition of the activated biosensing granules and again after two hours of granule addition.

The source for the active aerobic microbial consortia is raw sewage, or wastewater treatment plant or aerated sludge treatment unit.

The synthetic media used for growing the collected active aerobic microbial consortia consists of (in grams/liter): glucose – 30.0; ammonium chloride – 6.5; potassium dihydrogen

orthophosphate – 2.5; dipotassium hydrogen orthophosphate – 1.0; sodium bicarbonate – 5.5; yeast extract – 1.0; urea – 0.5; and tryptone – 1.0 at pH of $7.0 \pm$ is prepared, under aerated condition having air flow of 5 ml/minute, at 28°C for a period of 12 – 24 hours or till the mixed liquor suspended solids (MLSS) reaches 14500 – 15500 mg/liter on a dry weight basis.

Preferably, the biosensing granules are prepared by mixing microbial consortia of mixed liquor suspended solids (MLSS) 600 – 8500 mg/liter in 2 % (w/v) natural or synthetic polymer solution till it became a uniform mixture. This slurry is dropped into a 0.2 M curing solution in the form of droplets using a peristaltic pump to make uniform size granules of 1.0 to 1.5 mm diameter. These granules are cured at 4°C in 0.2M curing solution overnight and washed twice with water and then dried at room temperature.

Different industrial effluents from common effluent treatment plant mainly consisting of chemical industrial waste waters, textile industry effluents mainly consisting of H-acid and effluent from industries involved in extraction of natural products of plants are collected in bottles for the purpose of this invention. The collected effluents are characterised for their chemical oxygen demand and biological oxygen demand using classical methodologies.

Example 1:

Stable biosensing granule preparation:

The active aerobic microbial consortia was collected from wastewater treatment plant. The synthetic growth medium consisting of the following ingredients (in grams/liter): glucose – 30.0; ammonium chloride – 6.5; potassium dihydrogen orthophosphate – 2.5; dipotassium hydrogen orthophosphate – 1.0; sodium bicarbonate – 5.5; yeast extract – 1.0; urea – 0.5, and tryptone – 1.0 was prepared. The pH of the synthetic medium was adjusted to 7.0 using 0.1N hydrochloric acid or 0.1N sodium hydroxide solution. The collected microbial consortia was inoculated in the synthetic growth media and incubated under aerobic conditions with an air flow of 5 ml/minute, till the MLSS reached 15500 mg/l on dry weight basis at 28°C . The active microbial consortia was separated by centrifugation at 10000 rpm for 10 minutes at 28°C and the active microbial consortia slurry was prepared using 4% (w/v) active microbial consortia and 2% (w/v) sodium alginate solution in water. This slurry was then dropped in the form of droplets in 0.2M calcium chloride solution and the immobilised biosensing beads were further incubated in the same solution for a period of 18 hours at 4°C . The beads were then separated by draining the calcium chloride solution and washed repeatedly several times with water. The immobilised biosensing beads were then dehydrated at 28°C for 12 hours to obtain stable biosensing granules.

Example 2:

The active aerobic microbial consortia was collected from sewage treatment plant. The synthetic growth medium consisting of the following ingredients (in grams/liter): glucose – 30.0; ammonium chloride – 6.5; potassium dihydrogen orthophosphate – 2.5; dipotassium hydrogen orthophosphate – 1.0; sodium bicarbonate – 5.5; yeast extract – 1.0; urea – 0.5; and tryptone – 1.0 was prepared. The pH of the synthetic medium was adjusted to 7.0 using 0.1N hydrochloric acid or 0.1N sodium hydroxide solution. The collected microbial consortia was inoculated in the synthetic growth media and incubated under aerobic conditions with an air flow of 5 ml/minute, till the MLSS reached 14500 mg/l on dry weight basis at 30°C. The active microbial consortia was separated by centrifugation. The active microbial consortia slurry was prepared using 5% (w/v) active microbial consortia and 4% (w/v) sodium alginate solution in water. This slurry was then dropped in the form of droplets in 0.2M calcium chloride solution and the immobilised biosensing beads were further incubated in the same solution for a period of 12 hours at 4°C. The beads were then separated by draining the calcium chloride solution and washed repeatedly several times with water. The immobilised biosensing beads were then dehydrated at 24°C for 18 hours to obtain stable biosensing granules.

Example 3:

Active microbial consortia was collected from raw sewage. The synthetic growth medium consisting of following ingredients (in grams/liter): glucose – 30.0; ammonium chloride – 6.5; potassium dihydrogen orthophosphate – 2.5; dipotassium hydrogen orthophosphate – 1.0; sodium bicarbonate – 5.5; yeast extract – 1.0; urea – 0.5; and tryptone – 1.0 was prepared. The pH of the synthetic medium was adjusted to 7.0 using 0.1N hydrochloric acid or 0.1N sodium hydroxide solution. The collected microbial consortia was inoculated in the synthetic growth media and incubated under aerobic conditions with an air flow of 5 ml/minute, till the MLSS reached 15000 mg/l on dry weight basis at 28°C. The active microbial consortia was separated by centrifugation at 5000 rpm for 15 minutes at 28°C and the active microbial consortia slurry was prepared using 5% (w/v) active microbial consortia and 1% (w/v) sodium alginate solution in water. This slurry was then dropped in the form of droplets in 0.2M calcium chloride solution and the immobilised biosensing beads were further incubated in the same solution for a period of 24 hours at 4°C. The beads were then separated by draining the calcium chloride solution and washed repeatedly several times with water. The immobilised biosensing beads were then dehydrated at 30°C for 18 hours to obtain stable biosensing granules.

Example 4:**Characterisation of biosensing granules using synthetic medium**

The BOD and COD of the synthetic media were determined using standard methods prescribed by the American Public Health Association (APHA) (1967) Standard Methods for Examination of Water and Wastewater, Washington, DC. 300 ml of this synthetic media was taken in a standard BOD bottle and to this 0.2 grams of activated biosensing granules (BSG) were added. The dissolved oxygen concentration in the solution was measured at room temperature using dissolved oxygen probe.

S. No.	BOD ₅ (mg/l)	COD (mg/l)	BOD ₅ /COD	Dissolved oxygen consumed/2 hours by BSG (mg/l)
1	7410	9500	0.780	2.94
2	7450	9550	0.780	2.95
3	7350	9450	0.777	2.93

Example 5:**Characterisation of industrial common effluent using biosensing granules**

An effluent was collected from common effluent treatment plant, which consists of discharges from various industries. The effluent was characterised for COD and BOD₅ according to the procedure described by American Public Health Association (APHA) (1967) Standard Methods for Examination of Water and Wastewater, Washington, DC.

In a BOD bottle, 300 ml of the above effluent was taken and to this 0.2 grams of activated biosensing granules were added. The dissolved oxygen in the bottle was determined, at room temperature, initially and after two hours using dissolved oxygen probe.

S. No.	BOD ₅ (mg/l)	COD (mg/l)	BOD ₅ /COD	Dissolved oxygen consumed/2 hours by BSG (mg/l)
1	6440	10625	0.606	1.47
2	6340	10400	0.609	1.46
3	6540	10760	0.607	1.48

Example 6:**Characterisation of textile industry effluent using biosensing granules**

A textile industry effluent mainly consisting of H-acid was collected and characterised for COD and BOD₅ based on the procedure described by APHA (1967) Standard Methods for Examination of Water and Wastewater, Washington, DC. methods. In a BOD bottle, 300 ml of H-acid effluent was taken and to this 0.2 grams of activated

biosensing granules were added. The dissolved oxygen in the bottle was measured initially and after two hours, at room temperature, using dissolved oxygen probe.

S. No.	BOD ₅ (mg/l)	COD (mg/l)	BOD ₅ /COD	Dissolved oxygen consumed/2 hours by BSG (mg/l)
1	215	766	0.280	0.60
2	210	764	0.274	0.59
3	220	769	0.286	0.61

Example 7:

Characterisation of industrial effluent using biosensing granules

The effluent of an industry involved in extraction of natural products of plants was collected and analysed for various parameters like COD and BOD₅ using AHPA (1967) Standard Methods for Examination of Water and Wastewater, Washington, DC. procedures. In a BOD bottle, 300 ml of the above effluent was taken and to this 0.2 grams of activated biosensing granules were added. The dissolved oxygen in the bottle was measured initially and after two hours using dissolved oxygen probe at room temperature.

S. No.	BOD ₅ (mg/l)	COD (mg/l)	BOD ₅ /COD	Dissolved oxygen consumed/2 hours by BSG (mg/l)
1	7260	16200	0.448	0.84
2	7270	16250	0.447	0.82
3	7310	16340	0.447	0.86

Advantages of the invention:

The main advantages of this invention are:

1. The present invention provides a rapid methodology for characterisation of an effluent for its biotreatability.
2. The prepared stable biosensing granules can be stored at room temperature for a prolonged period without loss of activity.
3. The prepared stable biosensing granules can be reused several times for detection of biotreatability of an effluent.
4. The prepared biosensing granules are capable of being used in situ.
5. The prepared biosensing granules are easy to use and do not require specialised and/or skilled labour for use thereof.
6. The prepared biosensing granules of the invention render the detection of biotreatability of effluents cost effective.

7. The present invention for the detection of biotreatability of effluents by stable biosensing granules provides an easy and simple technique for effluent characterisation for their biotreatability.
8. The present invention for the detection of biotreatability of effluents by stable biosensing granules requires minimum precaution.
9. The present invention for the detection of biotreatability of effluents by stable biosensing granules can be used for the rapid evolution of biological degradable organic content in the effluent.
10. The present invention for the detection of biotreatability of effluents by stable biosensing granules does not require any additional inputs of chemicals for the characterisation of the effluent.
11. The invention is useful for the evaluation of large samples in a short time.
12. Any effluent can be characterised using the stable biosensing granules of the invention

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We claim:

1. A process for the preparation of stable and reusable biosensing granules useful in the assessment of biodegradability of effluents, said process comprising developing active aerobic microbial consortia in synthetic medium, separating the active aerobic microbial consortia, immobilising the said microbial consortia using a natural polymer to form biosensing granules, dehydrating the immobilised biosensing granules at 24 - 32°C for a period of 4 - 12 hours, to obtain stable biosensing granules having a moisture content of 5 - 30 %.
2. A process as claimed in claim 1 comprising
 - i. selecting a seed culture from raw sewage, wastewater treatment plants or activated sludge units;
 - ii. preparing a synthetic growth media;
 - iii. inoculating a microbial consortia in the said media;
 - iv. incubating the microbial consortia under aerobic condition having an air flow of about 5 ml/minute, at about 28°C for a period of 12 - 24 hours or till the level of mixed liquor suspended solids (MLSS) reaches 14500 - 15500 mg/liter on a dry weight basis;
 - v. separating the active aerobic microbial consortia by centrifugation at the appropriate rpm for 10 - 15 minutes and at a temperature of about 28°C,
 - vi. immobilizing the said microbial consortia using aqueous natural polymer solution by known methods to obtain immobilized biosensing beads;
 - vii. separating the said biosensing beads by decanting the said solution;
 - viii. washing the beads with water thoroughly several times;
 - ix. dehydrating the beads at a temperature in the range of 24 - 36°C for a period of 2 - 20 hours to obtain stable biosensing granules having a moisture content of 5 - 30 %;
 - x. activating the stable biosensing granules by incubation in 2 - 5 % (w/v) aqueous solution at 28°C for 2 - 10 hours to get active stable biosensing granules;
 - xi. separating the active granules from the activation solution by conventional methods.
3. A process as claimed in claim 1 wherein the aerobic microbial consortia is collected from raw sewage, wastewater treatment plants or from activated aerated sludge units.
4. A process as claimed in claim 1 wherein the synthetic growth media consists of (in grams/liter): glucose - 29 - 31; ammonium chloride - 5.5 - 7.5; potassium dihydrogen

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orthophosphate – 1.5 – 3.5; dipotassium hydrogen orthophosphate – 0.5 – 1.5; sodium bicarbonate – 4.5 – 5.5; yeast extract – 0.5 – 1.5; urea – 0.3 – 0.7; and tryptone – 0.5 – 1.5.

5. A process as claimed in claim 1 wherein the pH of the prepared synthetic growth media is adjusted to about 7.0 using 0.1 N hydrochloric acid or 0.1 N sodium hydroxide.
6. A process as claimed in claim 1 wherein about 10 % (w/v) of the collected microbial consortia is inoculated in the synthetic growth medium.
7. A process as claimed in claim 1 wherein the inoculated synthetic growth medium is aerated by passing air at the rate of about 5 ml/minute.
8. A process as claimed in claim 1 wherein the growth media is incubated at a temperature of 24 – 32°C.
9. A process as claimed in claim 1 wherein the growth of the active aerobic microbial consortia is terminated after the mixed liquor suspended solids (MLSS) reaches 14500 – 15500 mg/liter.
10. A process as claimed in claim 1 wherein the active aerobic microbial consortia is separated from the broth using conventional methods selected from centrifugation, settling, decanting the supernatant.
11. A process as claimed in claim 10 wherein the separated active aerobic microbial consortia is immobilized using 1 – 3 % (w/v) sodium alginate and 0.2M calcium chloride solution.
12. A process as claimed in claim 1 wherein the active aerobic microbial consortia is used for immobilisation in the range of 3 – 5 % (w/v) to obtain immobilized biosensing granules.
13. A process as claimed in claim 1 wherein the prepared immobilized biosensing granules are incubated for 12 – 24 hours at 4°C in 0.2 M calcium chloride solution.
14. A process as claimed in claim 1 wherein the prepared immobilized biosensing granules are separated from the calcium chloride solution by decanting the aqueous liquid.
15. A process as claimed in claim 1 wherein the immobilized biosensing granules are dehydrated at 24 – 32°C for a period of 2 – 20 hours to obtain stable biosensing granules with 5 – 30% moisture content.
16. A process as claimed in claim 1 wherein the stable biosensing granules are incubated for 2 – 10 hours in 2 – 5 % (w/v) glucose solution, at 24 – 32°C to obtain active stable biosensing granules.
17. A process as claimed in claim 1 wherein the stable biosensing granules are separated from the activation media by draining out the solution.

18. A process as claimed in claim 1 wherein the residual dissolved oxygen content of the effluent is measured using oxygen probe before and 2 – 6 hours of addition of activation stable biosensing granules in the range of from 2 – 5% (w/v).
19. A method for the estimation of the biotreatability of an effluent using the biosensing granules of claim 1 wherein the effluent is characterized as highly biotreatable if the dissolved oxygen consumption rate by the activated biosensing granules is more than 2 mg/l, medium when the said oxygen consumption rate is between 1.0 to 2.0 mg/l, and low when the oxygen consumption rate is less than 1.0 mg/l.

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ABSTRACT

The present invention provides a process for the preparation of stable and reusable biosensing granules useful in the assessment of biodegradability of effluents, said process comprising developing active aerobic microbial consortia in synthetic medium, separating the active aerobic microbial consortia, immobilising the said microbial consortia using natural polymer to form biosensing granules, dehydrating the immobilised biosensing granules to obtain stable biosensing granules having a moisture content of 5 – 30 %.